| Streamline flow | Turbulent flow |
| :--- | :--- |
| 1) The smooth flow of a fluid, with velocity <br> smaller than certain critical velocity (limiting <br> value of velocity) is called streamline flow or <br> laminar flow of a fluid. | 1) The irregular and unsteady flow of a fluid <br> when its velocity increases beyond critical <br> velocity is called turbulent flow. |
| 2) In a streamline flow, velocity of a fluid at a <br> given point is always constant. | 2) In a turbulent flow, the velocity of a fluid <br> at any point does not remain constant. |
| 3) Two streamlines can never intersect, i.e., they <br> are always parallel. | 3) In a turbulent flow, at some points, the <br> fluid may have rotational motion which <br> gives rise to eddies. |
| 4) Streamline flow over a plane surface can be <br> assumed to be divided into a number of plane <br> layers. In a flow of liquid through a pipe of <br> uniform cross sectional area, all the streamlines <br> will be parallel to the axis of the tube. | 4) A flow tube loses its order and particles <br> move in random direction. |

## Critical Velocity and Reynolds Number:

$R_{n}=\frac{V_{C} \rho d}{\eta}$ where $\mathrm{R}_{\mathrm{n}}=$ Reynolds number, $\mathrm{V}_{\mathrm{c}}=$ critical velocity, $\eta=$ coefficient of viscousity, $\rho=$ density of fluid, $d=$ diameter of tube
$R_{n}<1000$, streamline flow
$R_{n}>2000$, turbulent fluid
$1000<R_{n}<2000$, transition phase

## Viscosity:

Viscousity is the property by virtue of which, the relative motion between different layers of the fluid experience a dragging force In liquids drag is due to molecular cohesion and in gasses its due to collisions
In streamlline flow, Viscous drag is proportional to relative velocity. According to Newtons law of viscosity,

$$
\begin{aligned}
& f \alpha A \frac{d v}{d x} \\
& f=\eta A \frac{d v}{d x}
\end{aligned}
$$

Where $f=$ viscous force, $A=$ area of the layer, $\mathrm{dv} / \mathrm{dx}=$ velocity gradiet

 unit velocity gradient. S.I. Unit $\mathrm{Ns} / \mathrm{m}^{2}$

Note: Fluid with no drag => where every layer is moving with same velocity e.g.liquid helium at 2 K

## Stokes Law:

The viscous force Fv acting on a small sphere falling through a viscous medium is directly proportional to the radius of the sphere ( $r$ ), its relative velocity $(v)$ through the fluid, and the coefficient of viscosity( $\eta$ ) of the fluid

$$
\begin{aligned}
& F_{v} \alpha \eta r v \\
& F_{v}=6 \pi \eta r v
\end{aligned}
$$



## Terminal Velocity:

Consider a spherical body falling through a viscous fluid. The forces acting on it are
$\mathrm{mg}=\mathrm{V} . \rho \mathrm{s} . \mathrm{g}=4 / 3 \pi r^{3} \rho_{\mathrm{s}} \mathrm{g}=$ its weight (downward)
$\mathrm{U}=\mathrm{V} . \rho_{\mathrm{L}} \cdot \mathrm{g}=4 / 3 \pi r^{3} \rho_{\mathrm{L}} \mathrm{g}=$ upthrust (upwards)
$\mathrm{F}_{\mathrm{v}}=$ viscous force (upwards) $=6 \pi \eta r v$
Net downward force $=\mathrm{mg}-\mathrm{U}-\mathrm{Fv}$
till the net force exists velocity in downward direction keeps increasing and hence $F_{v}$ keeps increasing. There will be a moment when net force $=0$ and then the body will sink with a constant velocity (Since net force=0).
This contant velocity is called terminal velocity.
Then, $U+F_{v}=m g$
$\frac{4}{3} \pi r^{3} \rho_{L} g+6 \pi \eta r v=\frac{4}{3} \pi r^{3} \rho_{s} g$
Thus, $v=\frac{2}{9} \frac{r^{2} g\left(\rho_{S}-\rho_{L}\right)}{\eta}$

Law or Equation of continuity:


Let $\mathrm{v}_{1}$ speed of fluid at A and $\mathrm{v}_{2}$ be the speed of fluid at $B$
$A_{1}$ is the area of cross-section at $A$ and $A_{2}$ is the area of cross-section at $B$ (where $A_{2}<A_{1}$ )

Mass of fluid entering A in time $\Delta t=$ Mass of fluid exiting B in time $\Delta t$ $\rho$. (volume at $A$ in time $\Delta t)=\rho$. (volume at $B$ in time $\Delta t$ )
$\rho\left(A_{1} v_{1}\right)=\rho\left(A_{2} v_{2}\right)$
Thus, $\mathrm{A}_{1} \mathbf{v}_{1}=\mathrm{A}_{2} \mathbf{v}_{2} \mathbf{O R} \mathbf{A v}=$ constant
Thus smaller the area, greater is the velocity (assuming negligible friction and incompressible fluid)
NOTE: Av is called rate of flow or volume rate of flow or volume flux $\rho A v$ is called mass rate of flow or mass flux


Let $P_{1}$ be the pressure and $v_{1}$ be the velocity of the fluid at $P Q$ and $A_{1}$ the area of cross-section. Thus the force at this end is $\mathrm{P}_{1} \mathrm{~A}_{1}$.
Let $p_{2}$ be the pressure and $v_{2}$ be the velocity of the fluid at RS and $A_{2}$ the area of cross-section. Thus the force at this end is $p_{2} A_{2}$. Let $h=h_{2}-h_{1}$ be the difference is height.
Since $A_{2}<A_{1}, v_{2}>v_{1}$ (by principle of continuity), hence $d_{2}>d_{1}$ where $d_{1}$ and $d_{2}$ is the distance covered in time $\Delta t$
Thus, work done in time $\Delta t=W=p_{1} d_{1}-p_{2} \mathrm{dV}_{2}=p_{1} A_{1} d_{1}-p_{2} A_{2} d_{2}$
Note $d V_{1}=d V_{2}(=$ Volume in time $\Delta t)$. Thus, $\mathbf{W}=\left(\mathbf{P}_{1}-\mathbf{P}_{2}\right) \mathbf{d V}$....... (i)
But $\mathrm{W}=\Delta \mathrm{KE}+\Delta \mathrm{PE}$ where $\Delta \mathrm{KE}$ and $\Delta \mathrm{PE}$ are the change in time $\Delta \mathrm{t}$
$\Delta K E=1 / 2 m v_{2}{ }^{2}-1 / 2 m v_{1}{ }^{2}=1 / 2\left(\rho d V_{1}\right) v_{2}{ }^{2}-1 / 2\left(\rho d V_{2}\right) v_{1}{ }^{2}=1 / 2 \rho d V\left(v_{2}{ }^{2}-v_{1}{ }^{2}\right) . .(i i)$
$\Delta P E=m g h_{2}-m g h_{1}=\rho d V g\left(h_{2}-h_{1}\right) . . . . . . ~(i i i)$
Using (i), (ii) and (iii)
$\left(P_{1}-P_{2}\right) d V=1 / 2 \rho d V\left(v_{2}{ }^{2}-v_{1}{ }^{2}\right)+\rho d V g\left(h_{2}-h_{1}\right)$
Work done per unit volume of fluid by surrounding fluid is equal to sum of the change in KE \& PE per unit volume that occurs during the flow.
Thus, $P_{1}+1 / 2 \rho v_{1}{ }^{2}+\rho g h_{1}=P_{2}+1 / 2 \rho v_{2}{ }^{2}+\rho g h_{2}$
Thus, $P+1 / 2 \rho v^{2}+\rho g h=$ constant
Work done per unit volume of a fluid by the surrounding fluid is equal to the sum of the change in KE and PE per unit volume that occurs during the flow.

Applications:

- Efflux Velocity


NOTE: The efflux velocity is numerically same as the velocity of a point mass dropped from a height $h$.

## Ventury Meter/Ventury Tube



A ventury meter is used to measure the speed flow of a fluid.
$\rho=$ density of fluid
$A_{1}$ and $A_{2}=$ area of cross section of the tube
$v_{1}$ and $v_{2}=$ velocity of the fluid
By law of continuity, since A1>A2 thus v1<v2
From Bernoulli's principle,
$P_{1}+1 / 2 \rho v_{1}{ }^{2}+\rho g h_{1}=P_{2}+1 / 2 \rho v_{2}{ }^{2}+\rho g h_{2}$
Thus, $p_{1}-p_{2}=1 / 2 \rho\left(v_{2}{ }^{2}-v_{1}{ }^{2}\right)$
This difference in pressure creates a height difference in the tube
Thus, h $\rho \mathrm{g}=1 / 2 \rho\left(\mathrm{v}_{2}{ }^{2}-\mathrm{v}_{1}{ }^{2}\right)$
Since A1v1 = A2v2
$\mathrm{h} \rho \mathrm{g}=1 / 2 \rho\left(\left(\frac{\mathrm{~A}_{1} \mathrm{v}_{1}}{A_{2}}\right)^{2}-v_{1}^{2}\right)$
$2 g h=v_{1}^{2}\left(\left(\frac{A_{1}}{A_{2}}\right)^{2}-1\right)$
$v_{1}=\sqrt{\frac{2 g h}{\left(\frac{A_{1}}{A_{2}}\right)^{2}-1}}$

Lifitng of an Aeroplane


Due to the shape of the cross section of the wing the air is more crowded on top of the wing than below. Hence the speed of the wind is more
above. Hence by Bernoulli's principle the pressure on top is less than that below, due to which the plane gets an uplift (upward force called dynamic lift).

## Atomizer



Tube T is dipped in the liquid. Air at high speeds is blown over the tip of this tube with the help of a piston P. This high speed air creates a low pressure over the tube, due to which the liquid rises in it and is blow off in very small droplets with the expelled air. e.g. carburetor of an automobile engine, paint-gun, scent-spray, insectsprayer.

## Blowing off of roofs by stormy winds



The high speed winds creates a low pressure (p) above the roof (in accordance to Bernoulli's principle). Inside the room its still atmospheric pressure ( $\mathrm{p}_{\mathrm{o}}$ ). This difference in pressure will cause the roof to be lifted up and then blown away by the wind

## Ideal Fluid:

It is incompressible (density is constant)
Its flow is irrotational (no turbulance in flow)
It is nonviscous (no internal friction)
Has Steady flow (velocity at each point is constant in time)

## Properties of Fluid:

They do not oppose defomation completely(they get permantly deformed)
They have the ability to flow
They have ability to take shape of container

## Some terms:



Steady Flow : Measurable property like pressure or velocity of a fluid at a given point is constant over time.

Flow Line : Path of an individual particle in a moving fluid
StreamLine : A curve whose tangent at any point in the flow is in the direction of the velocity of the flow at that point. Streamlines and flow lines are identical for a steady flow.

Flow tube : It is an imaginary bundle of flow lines bound by an imaginary wall. For steay flow, the fluid cannot cross the walls of a flow tube. Fluids in adjacent flow tubes cannot mix.

Laminar Flow or Streamline Flow : It is a steady flow in which adjacent layers of a fluid move smoothly over each other.(Reynolds Number< 1000)

Turbulent flow : It is a flow at a very high flow rate. There is not steady flow and the flow pattern keeps changing. (Reynolds Number > 2000)

Hydrostatics: The branch of physics which deals with properties of fluids at rest

## VIII • IX • X ICSE • XI(Sc) • XII(Sc) • HSC/CET/JEE(M)/NEET(P \& C) • CBSE • IB • IGCSE • Engineering

